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The Zero Emission Power Plant Concept

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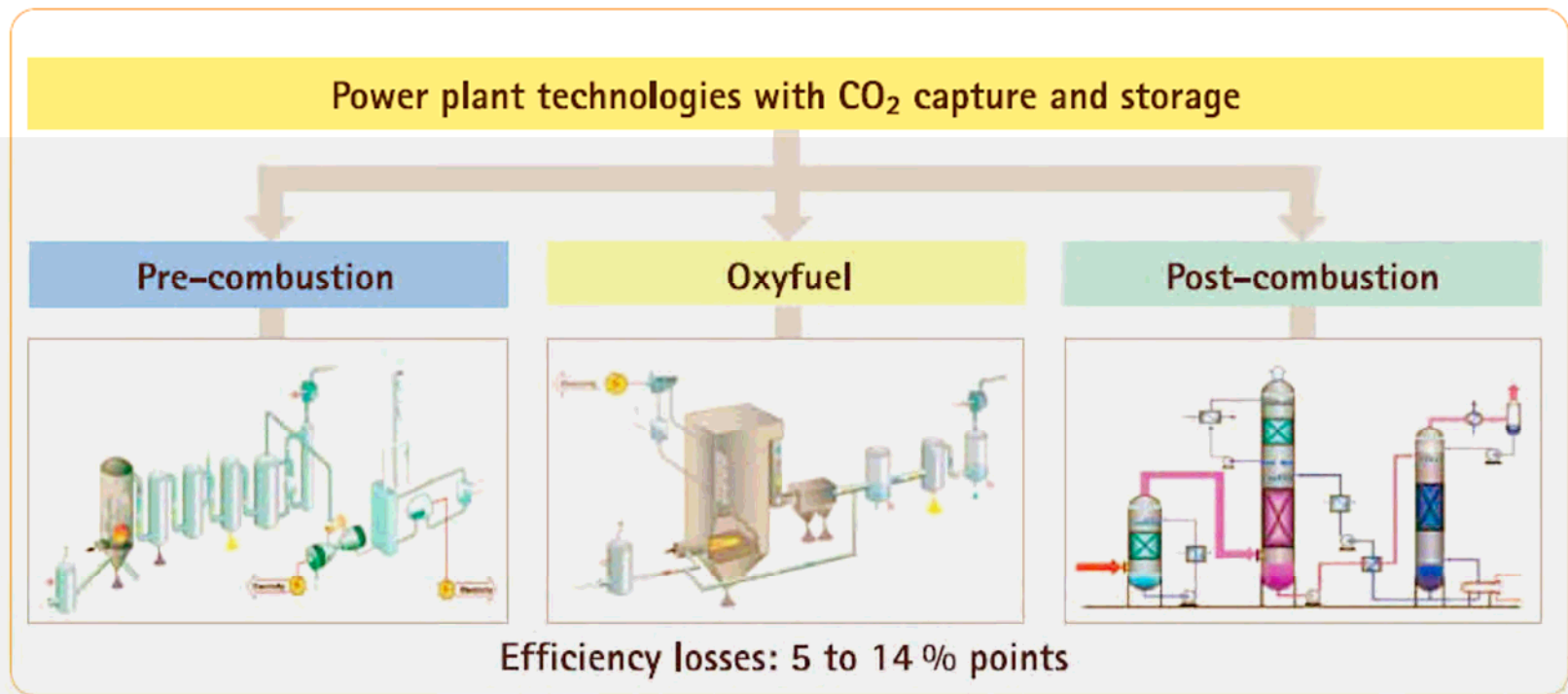
Introduction

- In the assessment report of IPCC it is stated that most of the observed global warming over the last 50 years is likely to have been due to the increase in GHG concentrations in the atmosphere. The IPCC further concludes that the stabilisation of the atmospheric CO₂ concentration requires CO₂ emissions to eventually drop well below current levels.
- In analysing CO₂ emissions reduction measures, it is concluded that none of the following measures alone is sufficient to stabilise CO₂ concentrations:
 - demand reductions and/or efficiency improvements
 - Increase of natural gas use
 - substitution among fossil fuels
 - switching to renewables or nuclear energy
 - CO₂ capture and sequestration
 - afforestation.
- At present, fossil fuels are the dominant source of the global primary energy demand, and will likely remain so for the rest of the century supplying over 85% of all primary energy, in spite of great efforts and investments made by many nations to increase the share of renewable energy to the primary energy demand and to foster conservation and efficiency improvements of fossil fuel usage.
- Capture and secure storage of CO₂ (CCS) allows the use of fossil fuels, while reducing atmospheric CO₂ emissions and mitigating global climate change.



CCS Technologies in Thermal Plants 1/5

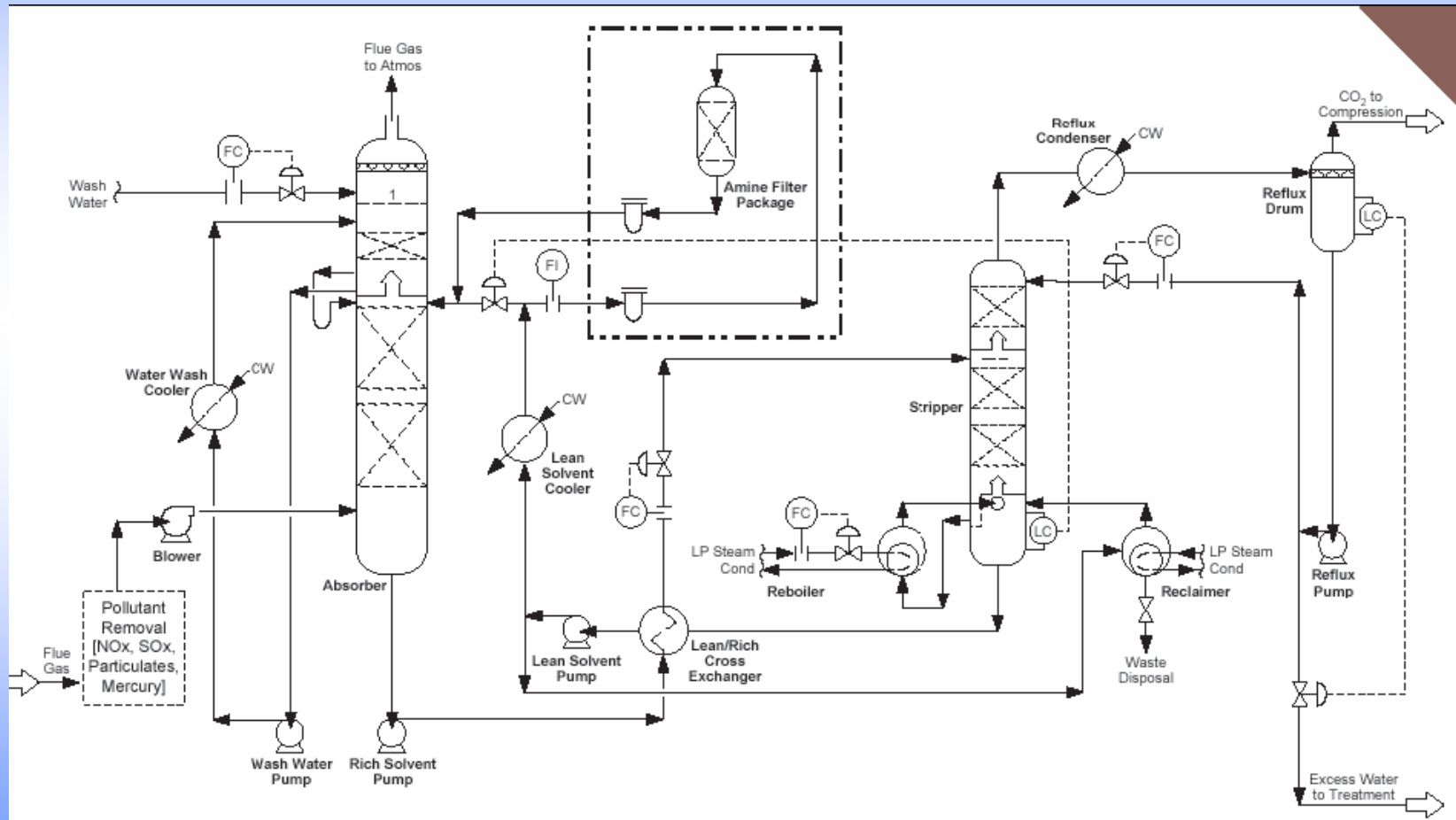
- The commercial or under development CO₂ sequestration technologies for coal-fired power plants can be divided into three broad categories:
 - Post combustion: separation of CO₂ from waste gas
 - Oxyfuel: combustion in O₂ instead of air
 - Pre-combustion: production of a carbon free fuel



Source: Alstom

CCS Technologies in Thermal Plants 2/5

CO₂ scrubbing from flue gas using amine solution

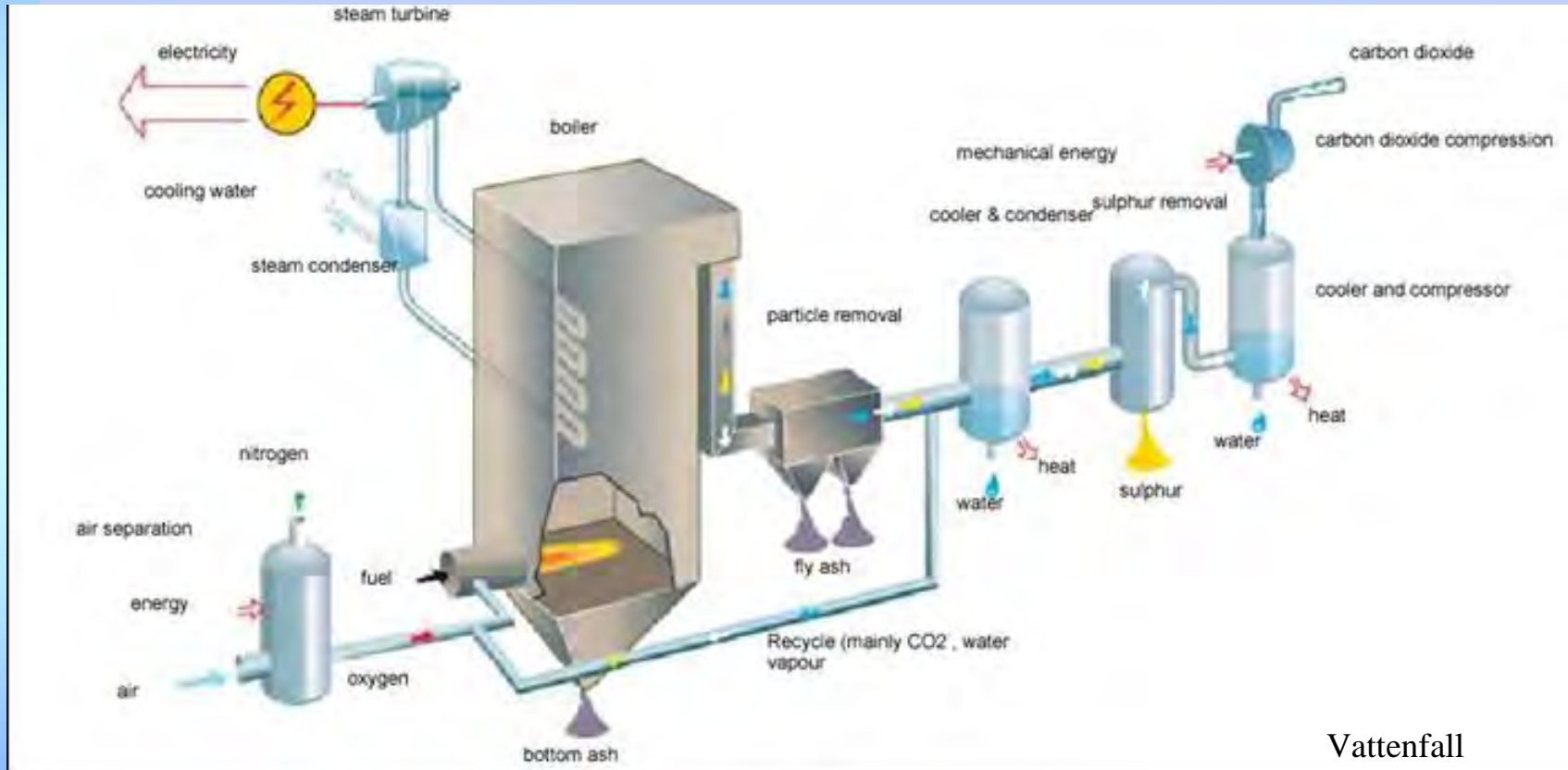


European Technology Platform, Zero Emission Fossil Fuel Power Plants (ZEP), Working Group 1, Power Plant and Carbon Dioxide Capture



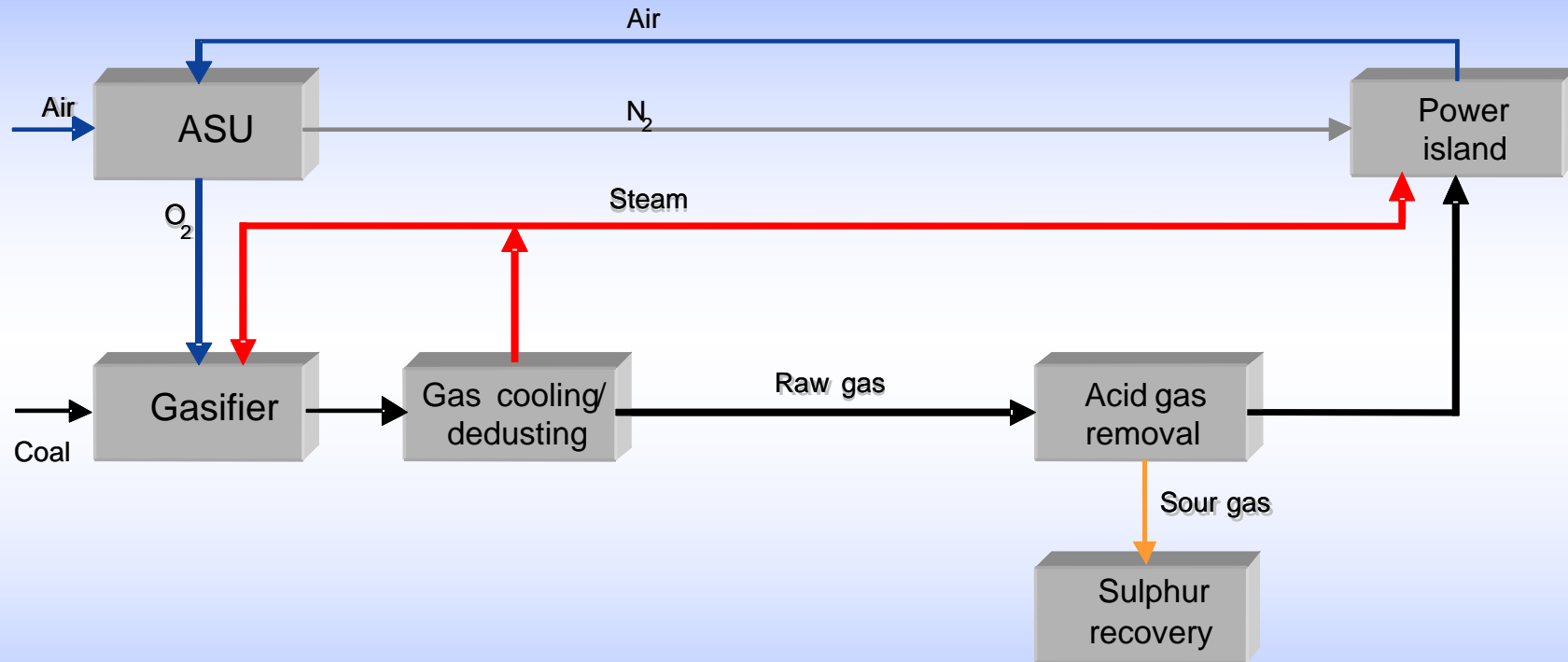
CCS Technologies in Thermal Plants 3/5

Oxyfuel combustion



CCS Technologies in Thermal Plants 4/5

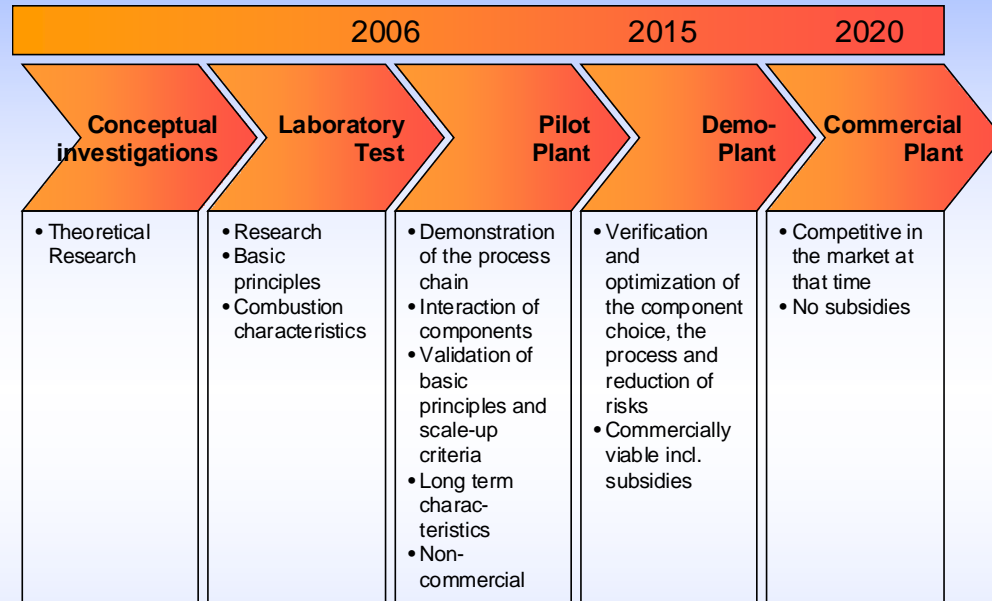
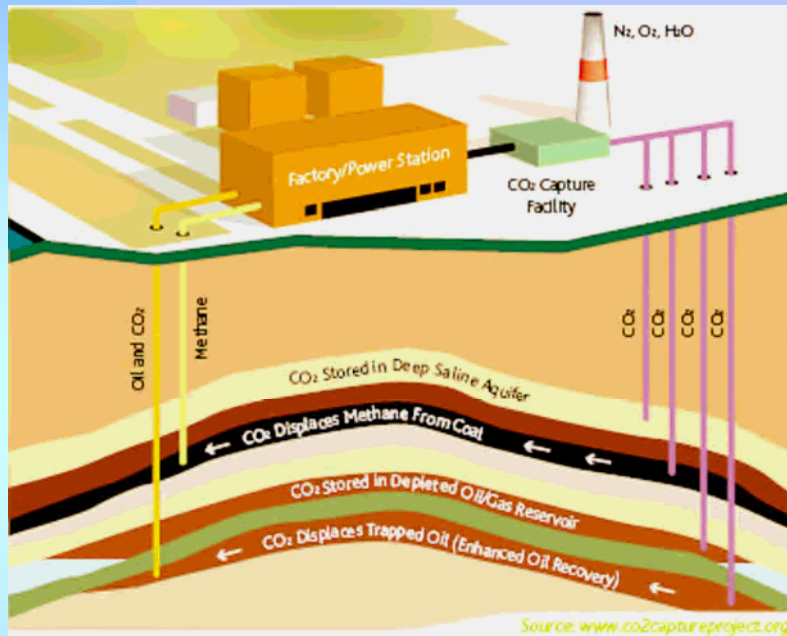
Production of a carbon free fuel



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CCS Technologies in Thermal Plants 5/5



CCS Technologies Time Frame

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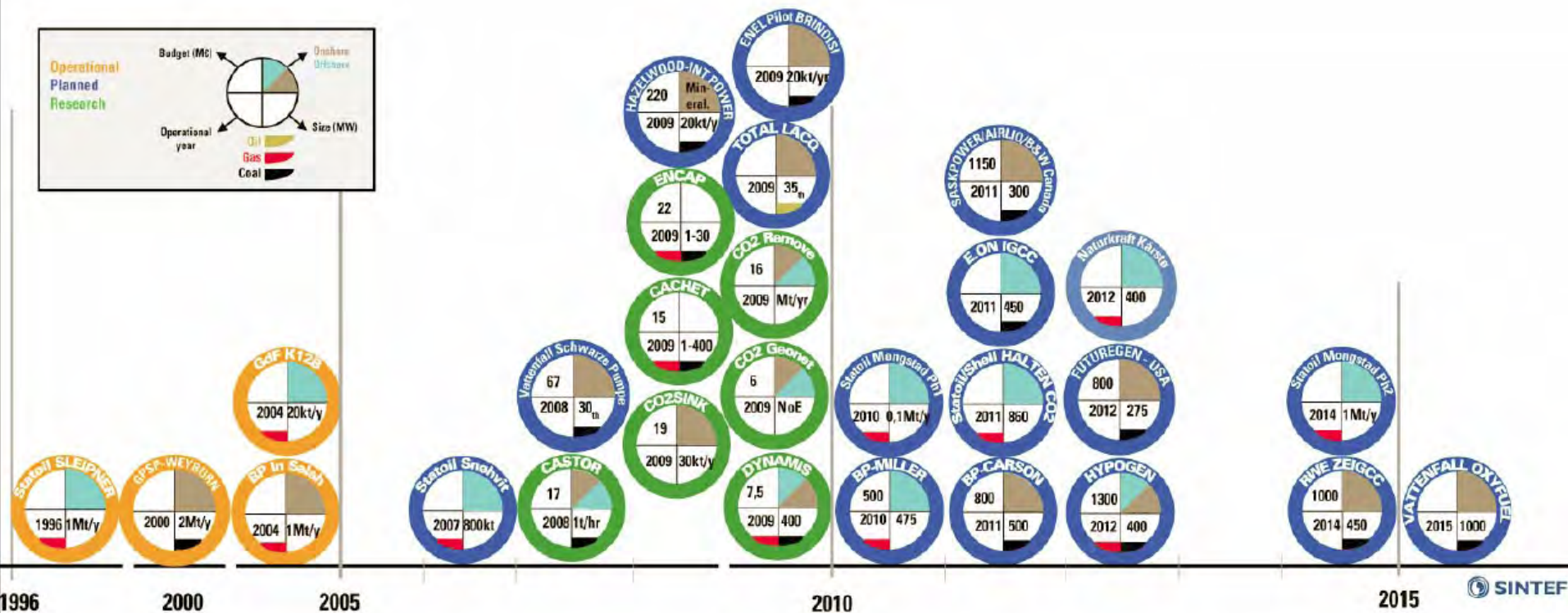


Research projects on the Zero Emission Power Plant

- CCS technologies in thermal PPs will contribute significantly in the mitigation of the GHG effect since thermal PPs account for ca. 1/3 of the total CO₂ atmospheric emissions. This fact explains the intense research activities aiming at the achievement of viable solutions in the medium term.
- Within FP6, the FENCO project aims at the development of the critical infrastructure for solid fuels, so that the EU technology remains competitive in the international market.
- The following are a number of important EC CCS projects with Greek partnership (NTUA - PPC):
 - ENCAP (Pre-combustion and oxyfuel technologies for solid fuels)
 - CASTOR (Post-combustion CO₂ capture)
 - CACHET (Post-combustion CO₂ capture for gaseous fuels)
 - ISSC (Production of a carbon-free gaseous fuel from solid fuels using CaO and pre-combustion CO₂ capture)
 - C2H (Production of a H₂-rich from solid fuels using CaO)



CCS pilot, demo and commercial projects



CCS in the European energy market 1/3

Coal		Reference Unit	Unit with pre-combustion capture	Unit with post-Combustion capture	Oxyfuel
Power output	MW	556	737	460	470
Efficiency	%	46	36	36	36
CO ₂ capture	%	-	92	85	91
EPC Capital cost	Euro/kW	918	1577	1446	1447
Lignite		Reference Unit	Unit with pre-combustion capture	Unit with post-Combustion capture	Oxyfuel
Power output	MW	920	717	731	760
Efficiency	%	43	41	39	41
CO ₂ capture	%	-	85	85	90
EPC Capital cost	Euro/kW	1065	1556	1683	1671
Natural Gas		Reference Unit	Unit with pre-combustion capture	Unit with post-Combustion capture	Oxyfuel
Power output	MW	420	755	662	325
Efficiency	%	58	41	47	48
CO ₂ capture	%	-	93	85	100
EPC Capital cost	Euro/kW	410	763	742	1124

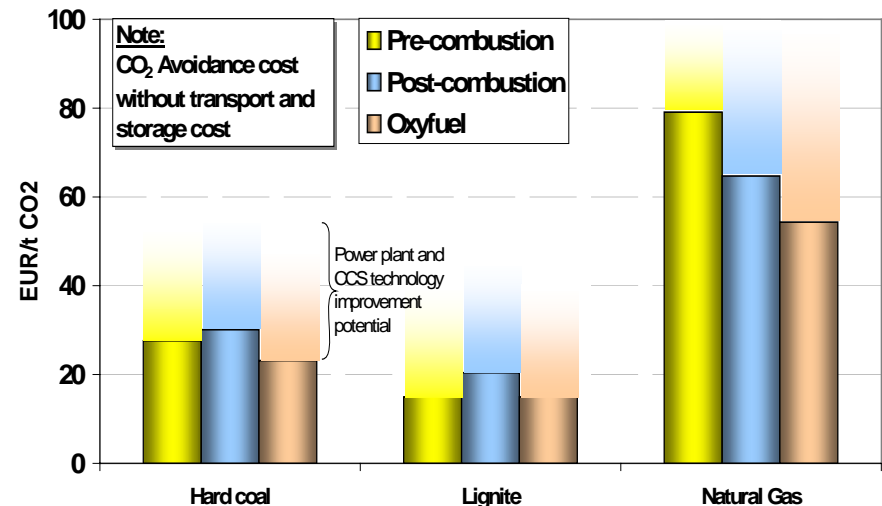
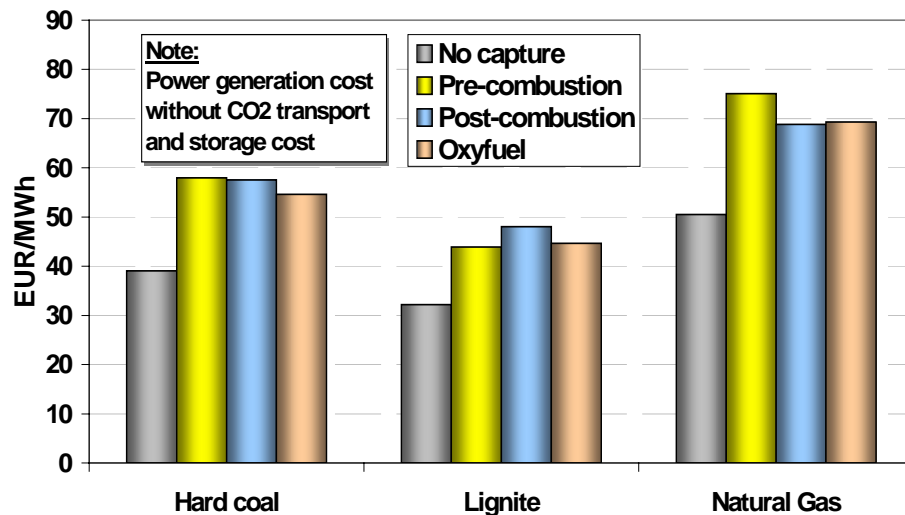
Financial and other Boundary Conditions		Natural Gas	Hard coal plant	Lignite plant
Economic life time	years	25	25	25
Depreciation	years	25	25	25
Fuel price	EUR/GJ (LHV)	5,8	2,3	1,1
Fuel price escalation	% per year	1,5%	1,5%	1,5%
Operating hours per year	hours per year	7500	7500	7500
Standard Emission factor	t/MWh _{th}	0,210	0,344	0,402
Common Inputs				
O&M cost escalation			2%	
Debt /Equity ratio	%		50%	
Loan interest rate	%		6%	
Interest during construction	%		6%	
Return on Equity	%		12%	
Tax rate	%		35%	
WACC			8%	
Discount rate	%		9,0%	

European Technology Platform, Zero Emission Fossil Fuel Power Plants (ZEP), Working Group 1, Power Plant and Carbon Dioxide Capture



CCS in the European energy market 2/3

Estimated electricity generation cost from large coal, lignite and natural gas PPs in 2020, without and with CO₂ capture



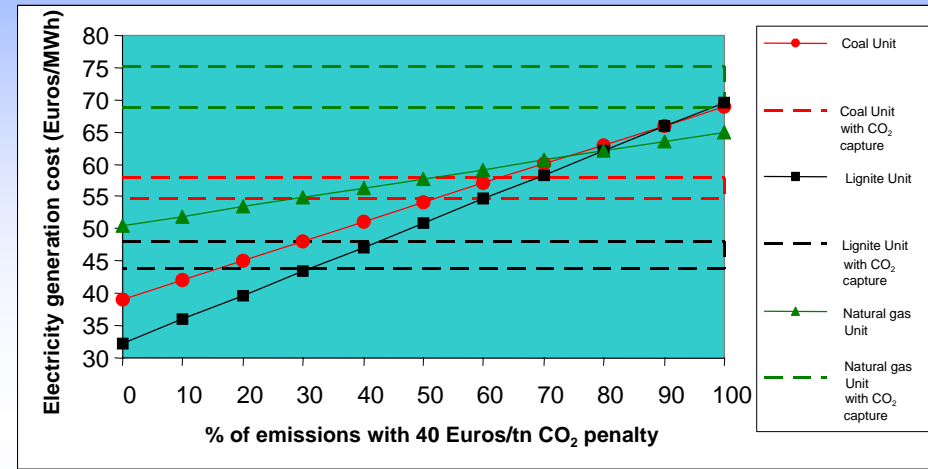
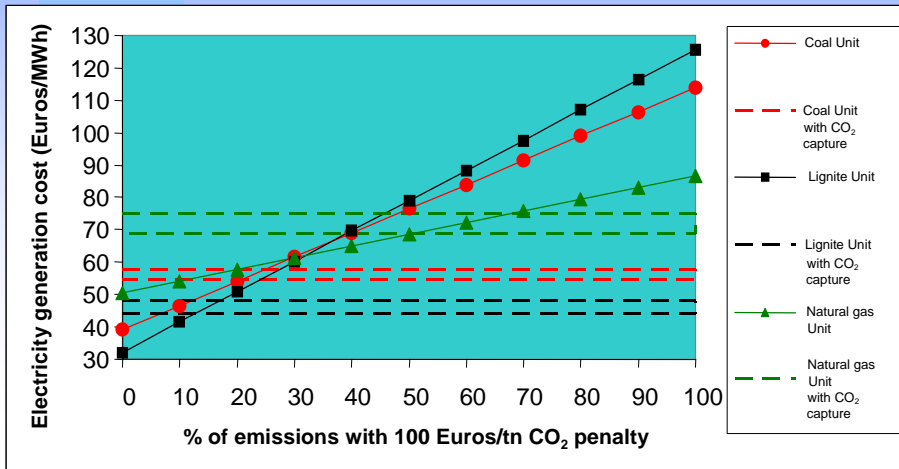
Estimated CO₂ capture cost from large coal, lignite and natural gas PPs in 2020, without and with CO₂ capture

European Technology Platform, Zero Emission Fossil Fuel Power Plants (ZEP), Working Group 1, Power Plant and Carbon Dioxide Capture



CCS in the European energy market 3/3

Electricity generation costs of large PPs with and without CO₂ capture/with CO₂ penalty in 2020



At the left of the point of intersection of the cost curves without and with CO₂ capture, investment in CCS technologies becomes economically viable

	Break-even point where CCS technologies become viable (% emissions)		
CO ₂ penalty (Euros/tn)	Coal	Lignite	Natural gas
100	23.5	14.2	56.9
40	58.8	35.6	>100



CO₂ Capture Retrofit in Greek Power Plants

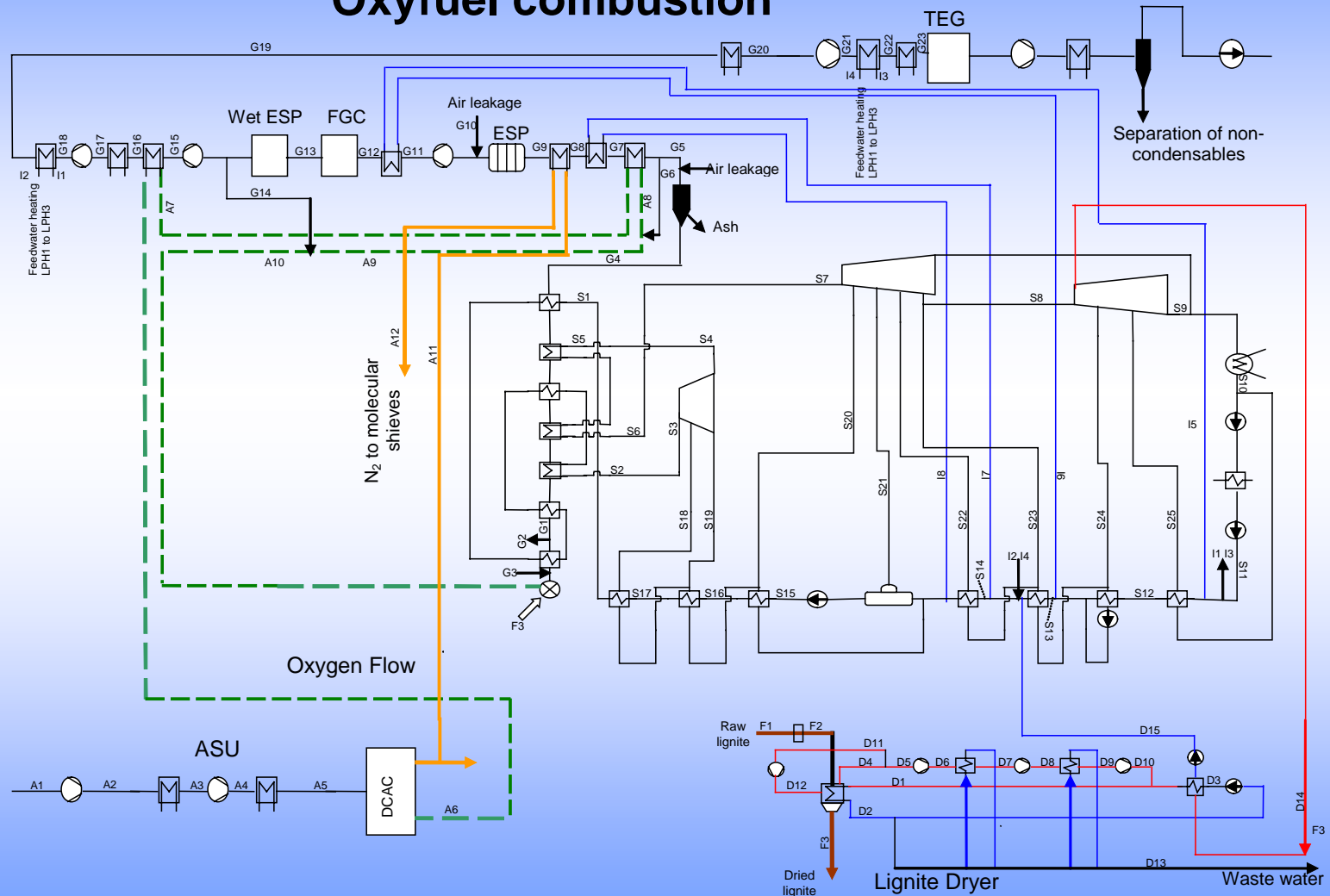
- In order to demonstrate the potential of CO₂ capture technologies for lignite applications, the simulation of a “typical” new 330 MW_{el} Greek PP was performed, including the retrofit options of amine scrubbing and Oxyfuel fuel firing. The PP has a supercritical boiler, a three pressure stage steam turbine and 8 regenerative feed water preheaters.

		Conventional PP	OxyFuel	Amine
Fuel Thermal Input	MW _{th}	830.0		
Thermal Consumption for Solvent Regeneration	MW _{th}	-	-	256.5
ASU Consumption	MW _{el}	-	58.1	-
CO ₂ Compression Consumption	MW _{el}	-	22.4	20.5
Cooling Pumps Consumption	MW _{el}	-	1.5	0.7
Power Consumption from Amine Scrubbing Unit	MW _{el}	-	-	8.7
Net Power Output	MW _{el}	293.7	211.0	200.5
Efficiency	%	35.74	25.42	24.16



Green-field Power Plants with CO₂ capture

Oxyfuel combustion



New 360 MWel Lignite PP with Oxyfuel combustion (typical Greek lignite)



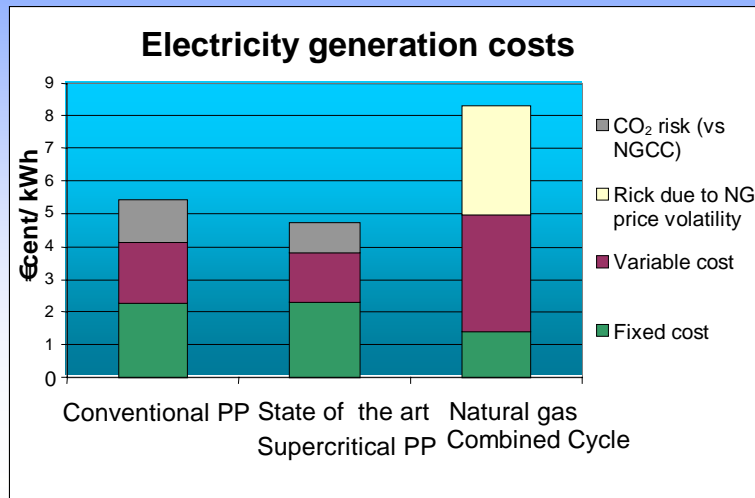
CCS in the Greek energy market 1/3

- The electricity generation cost has been assessed for the following technologies:
 - Conventional lignite PP
 - Conventional lignite PP with CO₂ capture with amine scrubbing
 - Conventional lignite PP with CO₂ capture with oxyfuel combustion
 - State of the art super-critical lignite PP (CCT)
 - Natural gas Combined Cycle (NGCC)
 - Lignite Integrated Gasification Combined Cycle (IGCC)
- The general and case-specific assumptions for the calculations are the following:
 - Discount factor: 8%, Inflation: 3%
 - Lignite cost: 1.8 €/ GJ, κόστος φυσικού αερίου: 5.5 €/GJ
 - Depreciation for Solid fuel units: 25 years, for NG and IGCC units: 15 years
 - O&M costs: 3% of capital costs per annually, variable cost 0.01 €/kWh for a lignite unit and 0.005 €/kWh for a natural gas unit.
 - 7500 h of operation per year at full load
 - CO₂ market cost: 18 €/tn

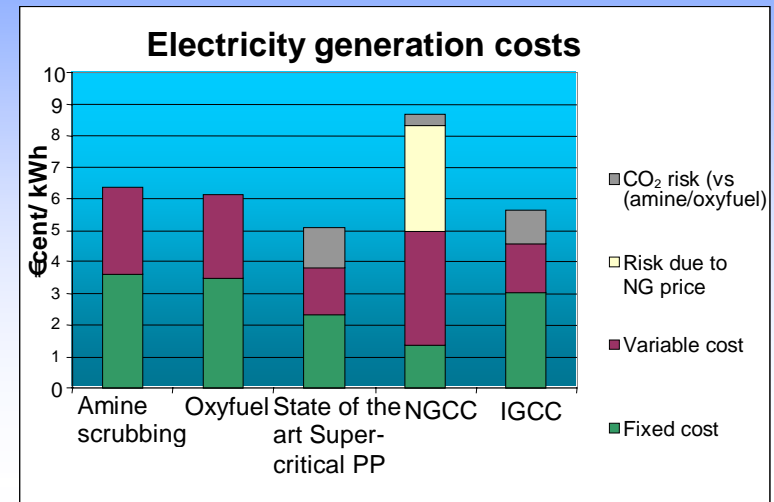
		Conv. lignite PP	Conventional lignite PP with amine scrubbing	Conventional lignite oxyfuel PP	State of the art super-critical lignite PP	NGCC.	IGCC
Net power output	MW _{el}	294	201	211	300	380	766
Efficiency	%	35.7	24.2	25.4	44.0	56.5	43.0
Capital cost	€/kW	1100	1900	1570	1150	600	1370
Specific CO ₂ emissions	kg/kWh	1.075	0.17	0.34	0.865	0.37	0.76



CCS in the Greek energy market 2/3



Electricity generation costs for current technologies



Electricity generation costs for future technologies

- Fixed cost includes depreciation and O&M costs, variable cost includes fuel.
- The units have been grouped in two categories: current technologies and technologies that will be commercially available in the future. The difference in specific emissions from the reference unit for each category multiplied by the CO₂ cost is an estimation of the price risk due to the emitted CO₂.



CCS in the Greek energy market 3/3

- The NGCC unit has the lowest fixed cost, due to the low capital cost, while on the other hand, the high capital and O&M costs for the units with CO₂ capture and the IGCC unit contribute significantly to the kWh cost.
- The lignite units, due to the low fuel price, demonstrate lower variable costs with respect to natural gas units.
- The low efficiency of units with CO₂ capture increases significantly variable costs.
- The increased volatility of NG price, due to its dependency to oil price (up to 40% of total costs) contributes in an increased uncertainty concerning the electricity generation cost from NGCC units, in contrast to the domestic local lignite market.
- The conventional lignite, the state of the art super-critical lignite and the IGCC units have the lowest kWh cost, while the NGCC unit has the highest generation cost, due to the high fuel price and the market volatility.
- The application of CCS technologies increases considerably capital costs and reduces efficiency and, as a consequence, increases electricity generation costs. Nevertheless, taking into account the CO₂ price, they can remain competitive.



Συμπεράσματα

- CCS technologies can contribute in the reduction of CO₂ emissions from the electricity generation sector.
- Nevertheless, the efficiency penalty and increased capital costs associated to the implementation of CCS technologies increase the kWh costs.
- In addition, the purchase of CO₂ credits from the through the CO₂, market is expected to increase electricity generation costs.
- From the assessment of different technological options for the Greek electricity sector, it is concluded that lignite units can be competitive to natural gas units, the latter presenting a greater market risk due to fuel price volatility.

